

Menno VAN DER BIJ - Deputy Manager Instrumentation Department

32th Annual European AIChE / Delta Process Academy Seminar

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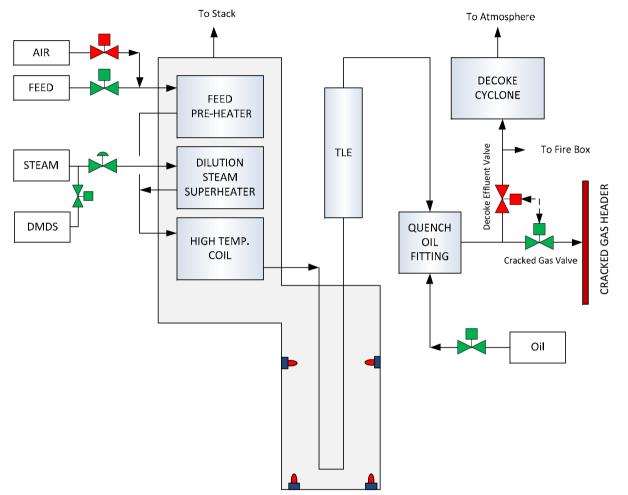
'Safe start-up of chemical plants' October 11th, 2016, Domein Martinus / Halle - Zoersel

AMERICAN INSTITUTE OF CHEMICAL ENGINEERS

Technip

Netherlands / Belgium Section

Switching between cracking and decoking Introduction



Cracking furnace in CRACKING mode of operation



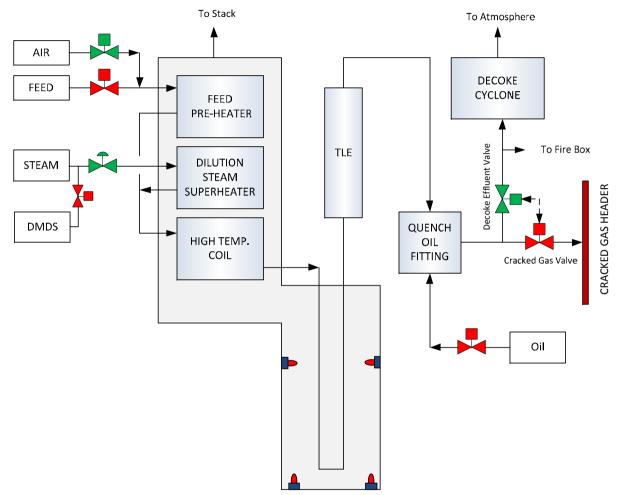
Switching between cracking and decoking Possible Hazards

While in CRACKING mode:

- Cracked gas leaking through decoke valve(s) to atmosphere
- Decoke air routed to furnace, mixing with HC
- High temperature downstream QOF in case of quench oil failure
- Backflow of cracked gas from header to cracking furnace in case of multiple radiant coil failure
- Low temperature downstream QOF due to failure of the emergency water back-up



Switching between cracking and decoking Introduction



Cracking furnace in **DECOKING** mode of operation



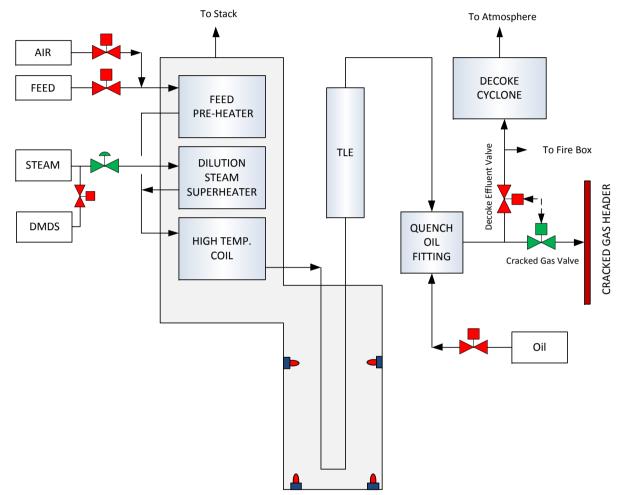
Switching between cracking and decoking Possible Hazards

While in **DECOKING** mode (open connection to atmosphere):

- Cracked gas leaking through cracked gas valve(s) to atmosphere
- Hydrocarbon feed routed to furnace, mixing with decoke air
- DMDS connected to atmosphere
- Quench oil connected to atmosphere
- Decoke effluent routed to cracked gas analyzer



Switching between cracking and decoking Introduction



Cracking furnace in HOT STANDBY mode of operation

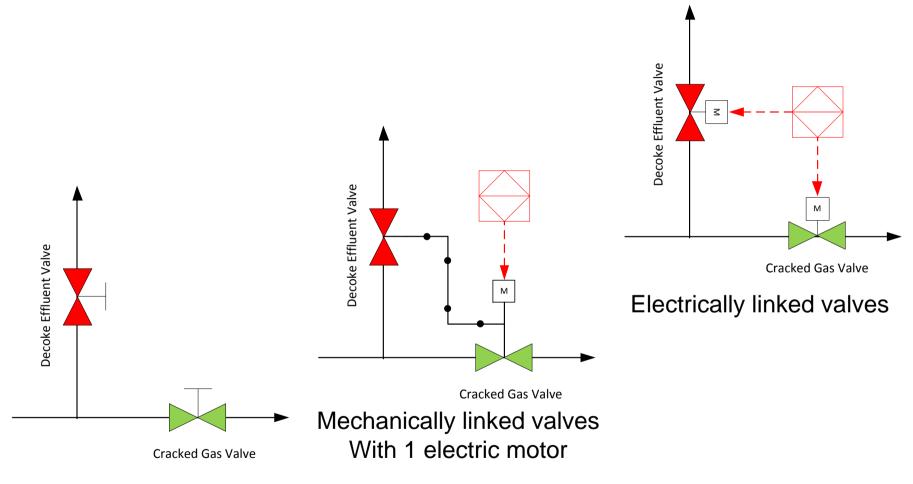


Switching between cracking and decoking Pre-conditions for change-over

- Hydrocarbon feed lines isolated
- Decoke air line isolated
- DMDS line isolated
- Quench oil line isolated
- Decoke air and HC feed lines purged with steam



Switching between cracking and decoking History



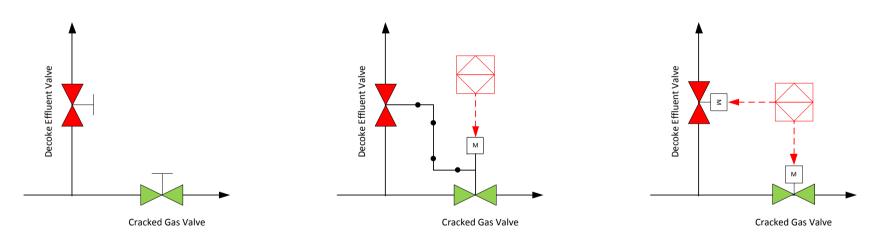
Individual operated valves



Switching between cracking and decoking Possible Hazards

During TRANSFER from cracking mode to decoking mode

- Overpressure due to simultaneously (partial) closed decoke and cracked gas valve(s)
- Backflow of cracked gas to atmosphere while both valves are open



Overpressure is possible in all 3 configurations

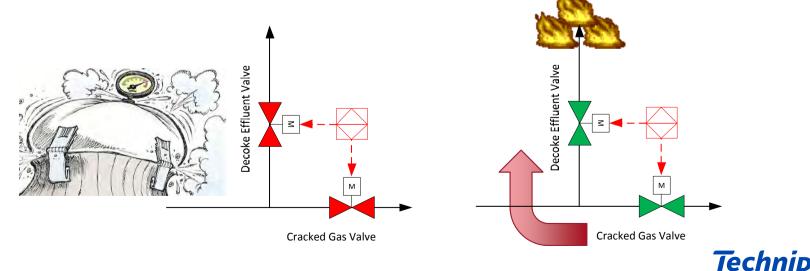


Switching between cracking and decoking Safety Instrumented System requirements

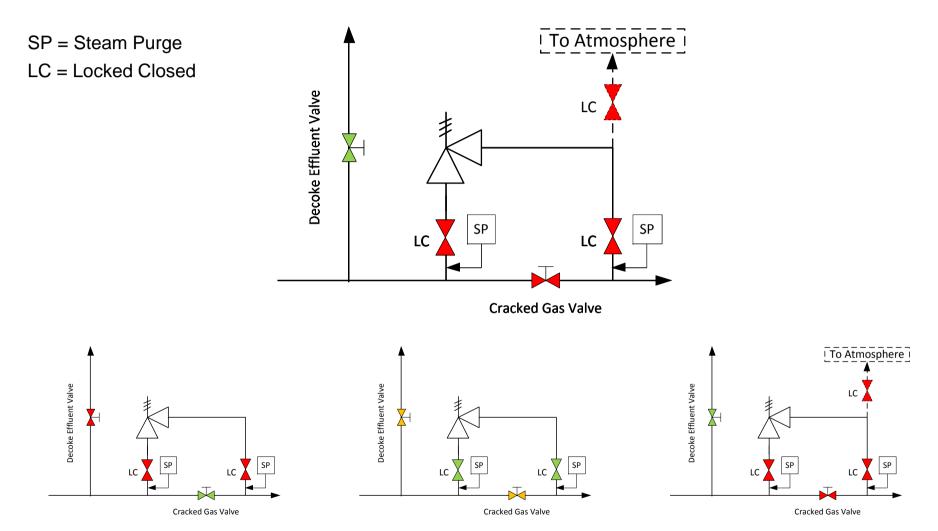
During TRANSFER from cracking mode to decoking mode



- Overpressure due to simultaneously (partial) closed decoke and cracked gas valve(s)
- Backflow of cracked gas to atmosphere

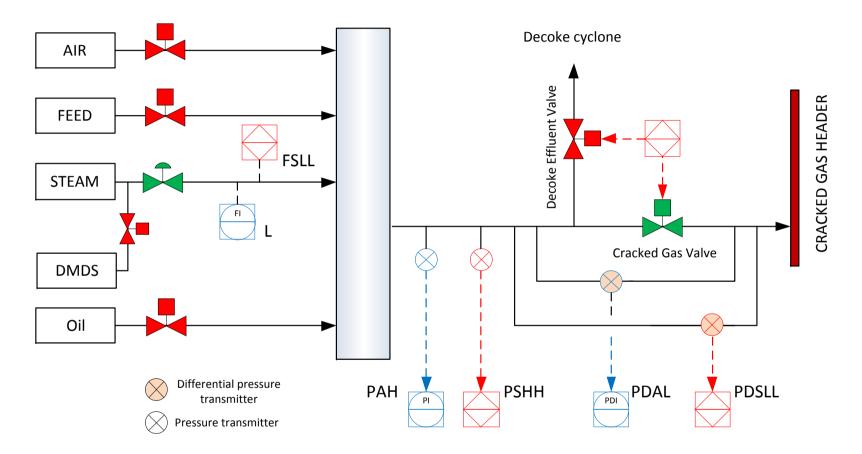


Switching between cracking and decoking Safety valve for overpressure protection





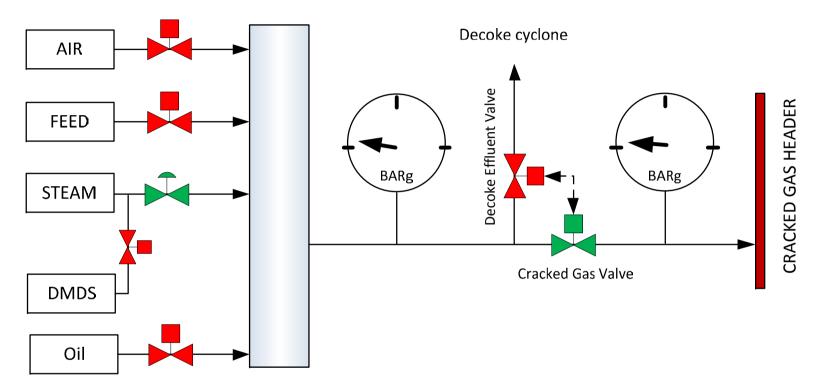
Switching between cracking and decoking Conceptual design



<u>Note</u>: Switch-over can be manually from local panel or DCS or fully automatic through the safeguarding system

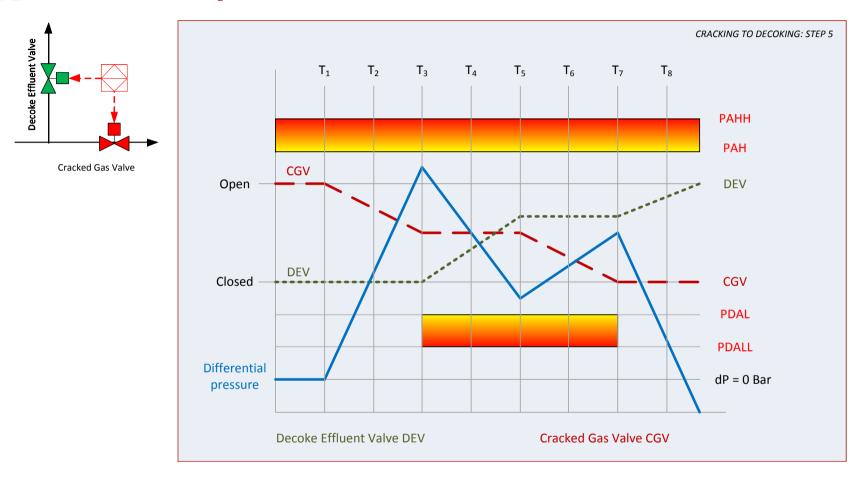


Switching between cracking and decoking Conceptual design



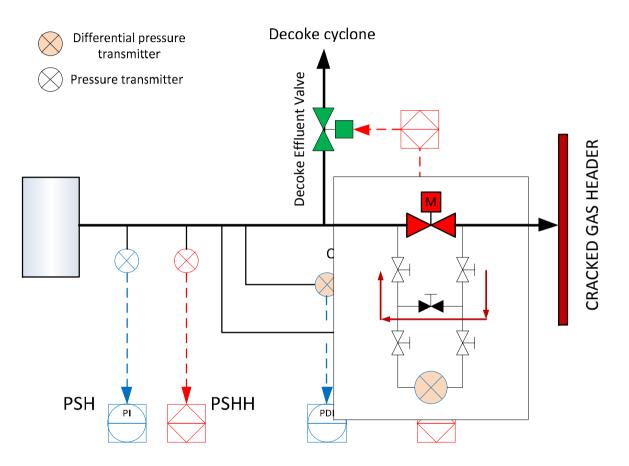


Switching between cracking and decoking Pressure profile



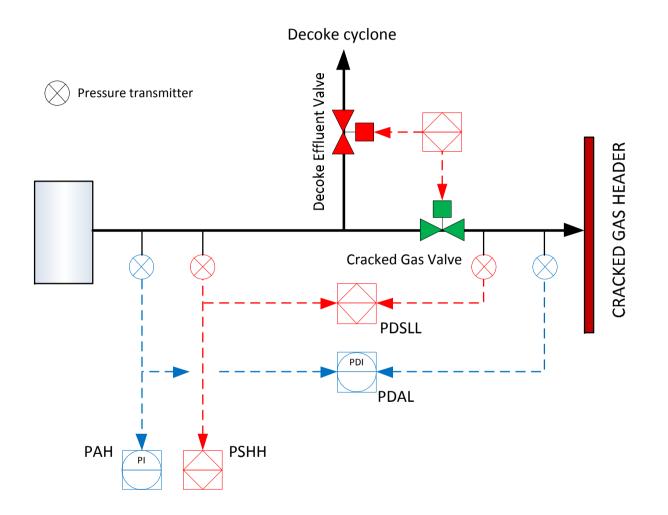


Switching between cracking and decoking Conceptual design



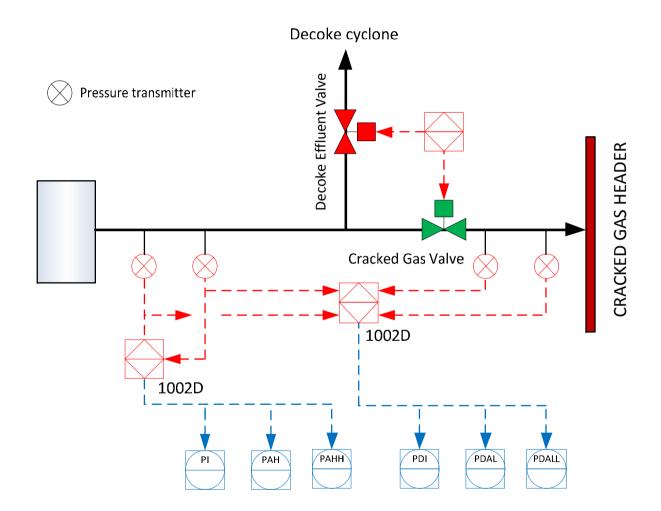


Switching between cracking and decoking Differential pressure transmitters replaced





Switching between cracking and decoking Improved reliability Safety Integrity Level





Switching between cracking and decoking Emergency isolation

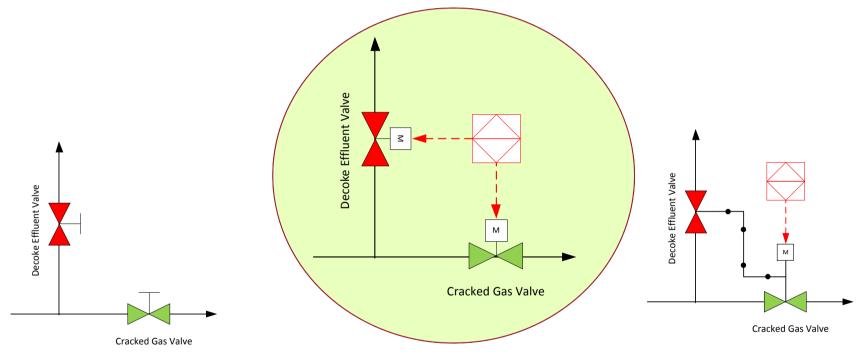
Closing the cracked gas valve after a multiple coil rupture

- Initiate furnace total shutdown:
 - > Close feed and DMDS valves
 - > Close decoke air valve
 - > Close fuel gas valves
- Close quench oil valve (if applicable)
- Overpressure protection remains active
- Steam purge of HC and decoke air lines bypassed



Switching between cracking and decoking Emergency isolation

Maintaining overpressure protection and preventing backflow of cracked gas to decoke drum only possible with electrically linked valves





Switching between cracking and decoking Conclusions

Advantages of electrically linked valves compared to mechanically linked valves

- Easier to install
- Easier to maintain pressures within safe limits
- Less dependent of dilution steam flow fluctuations
- Possibility for EMERGENCY ISOLATION after coil rupture while maintain overpressure and back flow protection



Switching between cracking and decoking Conclusions

Advantages of 4 gauge pressure transmitters compared to 2 dP-transmitters + 2 gauge transmitters

- Continuous comparison of transmitter availability
- Higher availability and reliability
- Less process connections = less steam purges
- No potential backflow over instrument equalization valve



Switching between cracking and decoking Conclusions

Advantages of overpressure protection with pressure transmitters compared to safety valve

- Overprotection always available
- Higher reliability no blocked PSV inlet
- No key-interlocks required



Switching between cracking and decoking

QUESTIONS ?





